Oil Emissions Factor Calc

A	В	с	D	E	F	G
'	•		•	•	•	
		From the carbon content of petrole	um and non-energy use	es to estimated	d emissions pe	er barrel
		•	Climate Mitigation Services		•	
ł			Rick Heede			
5			Carbon Majors Project 4-Jun-13	Copyrig	ght Climate Mitigatior	n Services
<u>}</u>			i sui i s			
- D						
1	Table 1	Pet	troleum & Natural Gas Liq	uids		
2			KgC/GJ	GJ/bbl	Kg carbon per bbl	Kg CO2 per bbl
4				I	• ·	•
5	Step 1:	Carbon in extracted oil	20.00	5.78	115.67	423.85
<u>6</u> 7	Step 2:	Adjust for natural gas liquids (NGLs) in reported production	100 percent	4.729%	110.20	403.80
8				_		
9	Step 3:	Inputs of own fuels to production, transportation, & processing	(applied in SummaryRanking.xls)		110.20	403.80
0 1	Step 4:	Vented carbon dioxide, oil operations	(applied in SummaryRanking.xls)		110.20	403.80
2	эсер н.			1	110.20	100.00
3	Step 5:	Fugitive, leaked, or vented methane	(applied in SummaryRanking.xls)	I	110.20	403.80
4	Chan Ca			-	110.00	102.00
<u>5</u> 6	Step 6:	Flaring at oil operations	(applied in SummaryRanking.xls)		110.20	403.80
7	Step 7:	Adjust for net carbon sequestered through non-fuel uses of oil	estimated in "non-energy uses" worksheet	8.018%	101.37	371.43
8						
9 0	Step 8:	Oxidation factor	100 percent		101.37	371.43
1	Step 9:	Convert step 8 factor to CO2e emissions per million barrels	Million tonnes Carbon and CO2	per million barrels	0.1014	0.3714
<u>2</u> 3	000000				0110111	
3						
4 5						
6 7	Table 2	IPCC net calorific value		TJ/Gg (TJ/kt; GJ/t) specific gravity		
<u>/</u> 3			158.99			computed percent C
9			136.7291	kg/bbl		84.60%
2				bbl /tonne		(F15/D37)
_				kgC/GJ, default C content IPCC GJ/bbl		
2			5.78	GJ/ JUI		
4			0.8600	UN, crude oil: specific gravity	Cumulative CM oil prod'n	984,657 Mbl
5				(unspecified origin)	Cumulative CM oil prod'n	134,631 Mt
6				Suriname (high)	Carbon content	113,898 Mt0
7			0.7240 UN (2012) Energy Statistics Yearbook 2009,	Indonesia (low)	Carbon sequestered	9,132 Mt0
. <u>8</u> .9			UN (2012) Energy Statistics Yearbook 2009, . 1,055.06			0.0508 tCC
0			1,033.00	o, 5 du		0.0506 tu

	К		м	N		0	Р	0		R		;	т	U		V	W	x		Y	Z	AA	AB	AC	AD
1	-1 12		1 10	1 1		- 1		×					•			· 1					<u> </u>	1,75		1 //0	1, 10
							haalia	round de	+	dafa	امر +ار	una fa	r oruda	مالمم	d notr	ماريم	nradua	+ o							
2	EIA / EPA background data on default values for crude oil ar														a petro	oleum	produc	ts							
3																									
4																									
5					Table A-249:	: Conversi	ion Factors	to Energy Units I	Heat Equi	valents)															
6					Fuel Category			Fuel Type			Р		Imports	Exports	Stock Change A	Adjustment	Bunkers	U.S. Territories							
8					Solid Fuels (M	fillion Btu	ı/Short Ton	) Anthracite C Bituminous (				22.57 23.89													
9								Sub-bitumino Lignite	us Coal			17.14 12.87				28.16 12.87									
10								Coke				12.07	25.00	25.63	25.00			25.14							
11					Natural Gas (	(BTU/Cub	ic Foot)	Unspecified				1,026	25.00	25.97	20.86	25.85		25.14 1,026							
12					Liquid Fuels	(Million B	tu/Barrel)	Crude Oil Nat Gas Liqu	ide and I R	Ge		5.80 3.69	5.99 3.69	5.80 3.69	5.80 3.69		5.80 3.69	5.80 3.69							
12								Other Liquid	5	.05		5.83	5.83	5.83	5.83	6.00	5.83	5.83							
14								Motor Gasoli Aviation Gas				5.22	5.22 5.05	5.22 5.05	5.22 5.05	5.22	5.22 5.05	5.22 5.05							
15								Kerosene Jet Fuel					5.67 5.67	5.67 5.67	5.67 5.67		5.67 5.55	5.67 5.67							
16								Distillate Fue Residual Oil	1				5.83 6.29	5.83 6.29	5.83 6.29	5.83 6.29	5.83 6.29	5.83							
17								Naphtha for p		cal feedstock	5		5.25	5.25	5.25		5.25	5.25							
18								Petroleum Co Other Oil for	petrochem	ical feedstoc	ks		6.02 5.83	6.02 5.83	6.02 5.83	6.02 5.83	6.02 5.83	6.02 5.83							
19								Special Naph Lubricants	thas				5.25 6.07	5.25 6.07	5.25 6.07		5.25 6.07	5.25 6.07							
20								Waxes Asphalt/Road	Oil				5.54	5.54 6.64	5.54		5.54	5.54							
21								Still Gas					6.00	6.00	6.00		6.00	6.00							
22					Data Sources: (	Coal and lig	gnite producti	Misc. Produc on: EIA (2010); Un		lid Fuels: EL	A (2011); Col	ke, Natural Ga	5.80 s and Petroleur	5.80 n Products: EL4	5.80 A (2011).		5.80	5.80							
23					US EP/	A (2011	) Invento	ory of U.S. Err	issions.	Annex 4	: IPCC Re	ference A	pproach f	or Estimat	ina CO2 E	missions	from Fossi	Fuel Comb	ustion						
24							,		,																
25		bon Content Coe					1000					2006	2007												
26	Fuel Type Petroleum		1990	1995 199						003 2004	• •		2007												
27	Asphalt and Road Aviation Gasolin		20.62 18.87	20.62 20. 18.87 18.	.62 20.62 .87 18.87	20.62 18.87	20.62 2 18.87 1	0.62 20.62 8.87 18.87	20.62 2 18.87 1	0.62 20.62 8.87 18.87	2 20.62 7 18.87	18.87	20.62 18.87												
28	Distillate Fuel Oi Jet Fuel <sup>a</sup>	1	19.95 19.40	19.95 19. 19.34 19.		19.95 19.33		9.95 19.95 9.33 19.33		9.95 19.95 9.33 19.33			19.95 19.33	Table A	56. Physi	cal Charac	teristics of	Liquefied P	etroleum	Gases					
29	Kerosene LPG (energy use)	) <sup>2</sup>	19.72 17.21	19.72 19. 17.20 17.		19.72 17.23		9.72 19.72 7.20 17.21		9.72 19.72 7.21 17.20		19.72	19.72 17.18	Table A	00. T Ny 31	cal onarad	1990-		Updated		0-2007	Updated	1990-2007	Update	ed
30	LPG (non-energy Lubricants	/ use) <sup>a</sup>	16.83 20.24	16.87 16. 20.24 20.	.86 16.88	16.88 20.24	16.84 1	6.81 16.83 0.24 20.24	16.82 1	6.84 16.81 0.24 20.24	16.81	16.78	16.76 20.24	Compo	und	Chemical	Densit		ensity	Ener		Energy	C Content	C Content	
31	Motor Gasoline <sup>a</sup>		19.41	19.38 19.	.36 19.35	19.33	19.33 1	9.34 19.34	19.35 1	9.33 19.33	19.33	19.33	19.33			Formula	(bbl / M	F) (bb	I / MT)	Cont (MMBt		Content MMBtu/bbl)	Coefficient (Tg C/QBtu)	Coefficient (1 C/QBtu)	ſġ
32	Residual Fuel Other Petroleun		21.49							1.49 21.49			21.49	Ethane		C <sub>2</sub> H <sub>6</sub>		6.88	11.55		2.916	3.082	16.25	17.1	
33	Av Gas Blend Co Mo Gas Blend Co		18.87 19.41	18.87 18. 19.38 19.	.36 19.35		19.33 1	8.87 18.87 9.34 19.34	19.35 1	8.87 18.87 9.33 19.33	19.33	19.33	18.87 19.33	Propane Isobutar		C <sub>3</sub> H <sub>8</sub> C <sub>4</sub> H <sub>10</sub>		2.44 1.20	12.76 11.42		3.824 4.162	3.836 3.974	17.20 17.75	16.7 17.7	
34	Crude Oil <sup>a</sup> Misc. Products <sup>a</sup>		20.16 20.16	20.23 20. 20.23 20.	.25 20.24	20.24 20.24	20.19 2 20.19 2	0.23 20.29 0.23 20.29	20.30 2	0.28 20.33	20.33	20.33 20.33	20.33 20.33	n-butane		C <sub>4</sub> H <sub>10</sub>	1	0.79	10.98		4.328	4.326	17.72	17.7	
35	Misc. Products (1	Terr.)	20.00 18.14	20.00 20.		20.00 18.14	20.00 2		20.00 2	0.00 20.00 8.14 18.14	20.00	20.00	20.00 18.14										EPA (2009b). All C). Values for n-		
136	Naphtha (<401 d					10.05	19.95 1	9.95 19.95 8.24 18.24	19.95 1	9.95 19.95 8.24 18.24	19.95	19.95	19.95 18.24					previous editi						sature are rot	
36	Naphtha (<401 d Other oil (>401 d Pentanes Phys	leg. F)	19.95	19.95 19.		19.95 18.24	18.24 1			9.37 19.37		19.37	19.37 27.85		U.S.	Environme	ental Prote	ction Agen	cy (2012	) Invento	ry of U.S.:	: 1990 - 201	0 Δnnex 2·		
37	Other oil (>401 d Pentanes Plus Petrochemical Fe	leg. F)	19.95 18.24 19.37	19.95 19. 18.24 18. 19.37 19.	.24 18.24 .37 19.37	18.24 19.37	19.37 1	9.37 19.37			37.05														
	Other oil (>401 d Pentanes Plus Petrochemical Fe Petroleum Coke Still Gas	leg. F)	19.95 18.24 19.37 27.85 17.51	19.95 19. 18.24 18. 19.37 19. 27.85 27. 17.51 17.	24 18.24 37 19.37 .85 27.85 .51 17.51	18.24 19.37 27.85 17.51	19.37 1 27.85 2 17.51 1	9.37 19.37 7.85 27.85 7.51 17.51	27.85 2 17.51 1	7.85 27.85 7.51 17.51	17.51	17.51	17.51					-		ied Petro	leum Gase	es, page A-87			
37 38	Other oil (≈401 d Pentanes Plus Petrochemical Fe Petroleum Coke Still Gas Special Naphtha Unfinished Oils <sup>a</sup>	leg. F)	19.95 18.24 19.37 27.85 17.51 19.86 20.16	19.95 19. 18.24 18. 19.37 19. 27.85 27. 17.51 17. 19.86 19. 20.23 20.	24 18.24 37 19.37 85 27.85 51 17.51 86 19.86 25 20.24	18.24 19.37 27.85 17.51 19.86 20.24	19.37 1 27.85 2 17.51 1 19.86 1 20.19 2	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86 0.23 20.29	27.85 2 17.51 1 19.86 1 20.30 2	7.85 27.85 7.51 17.51 9.86 19.86 0.28 20.33	17.51 19.86 20.33	17.51 19.86 20.33	17.51 19.86 20.33					-		ied Petro	leum Gase	es, page A-87			
37 38 39	Other oil (>401 d Pentanes Plus Petrochemical Fe Petroleum Coke Still Gas Special Naphtha	leg, F) æd.	19.95 18.24 19.37 27.85 17.51 19.86	19.95 19. 18.24 18. 19.37 19. 27.85 27. 17.51 17. 19.86 19.	24         18.24           37         19.37           85         27.85           51         17.51           86         19.86           25         20.24           81         19.81	18.24 19.37 27.85 17.51 19.86	19.37         1           27.85         2           17.51         1           19.86         1           20.19         2           19.81         1	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86	27.85 2 17.51 1 19.86 1 20.30 2 19.81 1	7.85 27.85 7.51 17.51 9.86 19.86	17.51 19.86 20.33 19.81	17.51 19.86 20.33 19.81	17.51 19.86					-		ied Petro	leum Gase	es, page A-87			
37 38 39 40 41 42	Other oil (~401 d Pentanes Plus Petrochemical Te Petroleum Coke Sill Gas Special Naphtha Unfinished Oils <sup>*</sup> Waxes Other Wax and M <sup>*</sup> C contents vary az	leg. F) ved. Misc. nnually based on ch	19.95 18.24 19.37 27.85 17.51 19.86 20.16 19.81 19.81 19.81	19.95 19. 18.24 18. 19.37 19. 27.85 27. 17.51 17. 19.86 19. 20.23 20. 19.81 19. 19.81 19. sition.	24         18.24           37         19.37           85         27.85           51         17.51           86         19.86           25         20.24           81         19.81           81         19.81	18.24 19.37 27.85 17.51 19.86 20.24 19.81 19.81	19.37         1           27.85         2           17.51         1           19.86         1           20.19         2           19.81         1           19.81         1	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86 0.23 20.29 9.81 19.81 9.81 19.81	27.85 2 17.51 1 19.86 1 20.30 2 19.81 1 19.81 1	7.85 27.85 7.51 17.51 9.86 19.86 0.28 20.33 9.81 19.81 9.81 19.81	17.51 19.86 20.33 19.81 19.81	17.51 19.86 20.33 19.81 19.81	17.51 19.86 20.33 19.81 19.81					-		ied Petro	leum Gase	es, page A-87			
37 38 39 40 41 42 43	Other oil (~401 d Pentanes Plus Petrochemical Fe Petroleum Coke Still Gas Special Naphtha Unfinished Oils <sup>a</sup> Waxes Other Wax and M <sup>*</sup> C contents vary at <sup>*</sup> C content for utili fuel is burned. Co:	ieg. F) eed. <u>Misc.</u> nnually based on chi- ity coal used in the e al, crude oil, and nat	19.95 18.24 19.37 27.85 17.51 19.86 20.16 19.81 19.81 19.81 19.81 19.81 ung as in fuel compo lectric power calculu ural gas all include of	19.95 19. 18.24 18. 19.37 19. 27.85 27. 17.51 17. 19.86 19. 20.23 20. 19.81 19. 19.81 19. sition. attoms. All coefficients of the second se	24 18.24 37 19.37 85 27.85 51 17.51 86 19.86 25 20.24 81 19.81 .81 19.81 .19.81 .19.81 .19.81 .19.81	18.24 19.37 27.85 17.51 19.86 20.24 19.81 19.81 gher heating hydrogen. V	19.37 1 27.85 2 17.51 1 19.86 1 20.19 2 19.81 1 19.81 1 19.81 1	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86 0.23 20.29 9.81 19.81 9.81 19.81 r heating value (grossels are burned, the c	27.85 2 17.51 1 19.86 1 20.30 2 19.81 1 19.81 1 19.81 1 s heating va arbon and h	7.85 27.85 7.51 17.51 9.86 19.86 0.28 20.33 9.81 19.81 9.81 19.81 9.81 19.81 ydrogen comb	17.51 19.86 20.33 19.81 19.81 19.81 amount of P	17.51 19.86 20.33 19.81 19.81 teat released w gen in the air to	17.51 19.86 20.33 19.81 <u>19.81</u> then a					-		ied Petro	leum Gase	es, page A-87			
37 38 39 40 41 42 43 44	Other oil (~401 di Pentanes Phus Petrochemical Fe Petroleum Coke Still Gas Special Naphtha Unfinished Oths <sup>4</sup> Waxes <u>Other Wax and M</u> <sup>7</sup> C contents vary ar <sup>9</sup> C content for unih feal is burned. Co: CO <sub>2</sub> and water. So	leg. F) eed. Innually based on chi tiy coal used in the e al, crude oil, and nat me of the energy re Lower heating valu	19.95 18.24 19.37 27.85 17.51 19.86 20.16 19.81 19.81 19.81 19.81 ural gas all include c ieased in burning go ie (net heating value	19.95 19. 18.24 18. 19.37 19. 27.85 27. 17.51 17. 19.86 19. 20.23 20. 19.81 19. 19.81 19. 19.81 19. ition. All coeffic chemical compour es into transformi s in contrast, doe	24 18.24 37 19.37 85 27.85 51 17.51 .86 19.86 25 20.24 81 19.81 .81 19.81 .19.85 .19.8	18.24 19.37 27.85 17.51 19.86 20.24 19.81 19.81 19.81 thydrogen. V steam and is steam and is	19.37 1 27.85 2 17.51 1 19.86 1 20.19 2 19.81 1 19.81 1 19.81 1 value. Highe When those fu is usually lost. transforming	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86 0.23 20.29 9.81 19.81 9.81 19.81 9.81 19.81 r heating value (gros els are burned, the c The amount of heat the water into steam	27.85 2 17.51 1 19.86 1 20.30 2 19.81 1 19.81 1 s heating va arbon and hypent in tran	7.85 27.85 7.51 17.51 9.86 19.86 0.28 20.33 9.81 19.81 9.81 19.81 9.81 19.81 sforming the tota sforming the top	17.51 19.86 20.33 19.81 19.81 19.81 anount of P ine with oxyg water into step odology based	17.51 19.86 20.33 19.81 19.81 theat released w gen in the air to am is counted a d on Internation	17.51 19.86 20.33 19.81 <u>19.81</u> then a produce as part of nal					-		ied Petro	leum Gase	es, page A-87			
37 38 39 40 41 42 43 44 45	Other oil (~401 di Pentanes Phus Petrochemical Fe Petroleum Coke Still Gas Special Naphtha Unfinished Otis <sup>4</sup> Waxes <u>Other Wax and N</u> <sup>1</sup> C contents vary ar <sup>1</sup> C content for utili field is burned. Co: CO <sub>2</sub> and water. So gross heat content Energy Agency de	leg. F) eed. Innually based on chi tiy coal used in the e al, crude oil, and nat me of the energy re Lower heating valu	19.95 18.24 19.37 27.85 17.51 19.86 20.16 19.81 19.81 19.81 anges in fuel compo- lectric power calcul- ural gas all include c tensed in burning go te (net heating value g value can be conv	19.95 19, 18.24 18, 19.37 19, 27.85 27, 17.51 17, 19.86 19, 20.23 20, 19.81 19, 20.23 19, 19.81 19, 19.81 19, ition. All coeffici- hemical compoun- es into transformi ), in contrast, doe	24 18.24 37 19.37 85 27.85 51 17.51 86 19.86 25 20.24 81 19.81 81 19.81 einst based on high and of carbon and ing the water into a so to include the h	18.24 19.37 27.85 17.51 19.86 20.24 19.81 19.81 19.81 thydrogen. V steam and is heat spent in al and petrole	19.37 1 27.85 2 17.51 1 19.86 1 20.19 2 19.81 1 19.81 1 value. Higher When those fut a usually lost. transforming eum products	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86 0.23 20.29 9.81 19.81 9.81 19.81 r heating value (groo: els are burned, the c The amount of heat	27.85 2 17.51 1 19.86 1 20.30 2 19.81 1 19.81 1 s heating va arbon and hypent in tran	7.85 27.85 7.51 17.51 9.86 19.86 0.28 20.33 9.81 19.81 9.81 19.81 9.81 19.81 sforming the tota sforming the top	17.51 19.86 20.33 19.81 19.81 19.81 anount of P ine with oxyg water into step odology based	17.51 19.86 20.33 19.81 19.81 theat released w gen in the air to am is counted a d on Internation	17.51 19.86 20.33 19.81 <u>19.81</u> then a produce as part of nal					-		ied Petro	leum Gase	es, page A-87			
37 38 39 40 41 42 43 44 45 46	Other oil (<401 di Pentanes Phus Petrochemical Fe Petroleum Coke Silil Gas Special Naphtha Unfinished Oils* Waxes Other Wax and A 'C content for unit feal is burned. Coc Co <sub>3</sub> and water. So gross bact content Energy Agency de coefficients are pro-	leg. F) seed. mmally based on che ity coal uwed in the e ity coal uwed in the e ity coal used in the e ity coal used in the sentence of the energy re- Lower heating vah sfaults, higher heatin esented in higher heatin	19.95 18.24 19.37 27.85 17.51 19.86 20.16 19.81 19.81 anges in fuel compo lectric power calcul und gas all include ( seased in burning go les (path barling value g value can be conv ating value because	19.95 19 18.24 18: 19.37 19. 27.85 27. 17.51 17. 19.86 19. 20.23 20. 19.81 19. ition. All coeffic chemical compou s into transformi ), in contrast, doe erted to lower her U.S. energy statis	24         18.24           37         19.37           85         27.85           51         17.51           86         19.86           25         20.24           81         19.81           81         19.81           stort include the h atting value for coal tics are reported by	18.24 19.37 27.85 17.51 19.86 20.24 19.81 19.81 19.81 thydrogen. V steam and is heat spent in al and pet in by higher heat	19.37 1 27.85 2 17.51 1 19.86 1 20.19 2 19.81 1 19.81 1 19.81 1 19.81 1 walue. Higher When those for susually lost. transforming eum products ating value.	9.37 19.37 7.85 27.85 7.51 17.51 9.86 19.86 0.23 20.29 9.81 19.81 9.81 19.81 9.81 19.81 9.81 19.81 r heating value (groz els are burned, the c the water into steam by multiplying by 0	27.85 2 17.51 1 19.86 1 20.30 2 19.81 1 19.81 1 s heating va arbon and hy spent in tran Using a sin 95 and for r	7.85 27.85 7.51 17.51 9.86 19.86 0.28 20.33 9.81 19.81 9.81 19.81 9.81 19.81 ydrogen comb sforming the tott ydrogen comb	17.51 19.86 20.33 19.81 19.81 19.81 al amount of h ine with oxyg water into stee multiplying b	17.51 19.86 20.33 19.81 19.81 19.81 don Internation of On Internation y 0.90. Carbon	17.51 19.86 20.33 19.81 <u>19.81</u> <u>19.81</u> <u>19.81</u> <u>as part of mal</u> n content	coione from	table	• A-56: Ph	ysical Char	-		ied Petro	leum Gase	es, page A-87			
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AE	AF		AG	AH		Al		AJ	AK		AL		AM	AN	AC	D	AP	A	2	AR		AS	AT	AU		AV	AW	Π
							IP	CC ba	ckgrc	ound	data	on de	efault v	alues fo	or crud	le oil	and pe	troleu	m pro	oducts								
-																												
7	[											_									I	DEFAULT VAL	TABLE 1.3 UES OF CAR	BON CONTEN	r			
		Dr	FAULT EMISS	(kg of gree	RS FOR STATI		a net calo		RGY INDUST									Fuel ty	pe Englisl	h description	l			Default carb content <sup>1</sup> (kg/GJ)		Lower	Upper	
-				CO2			CH4			N <sub>2</sub> O		_						Crude (	Dil					20.0		19.4	20.6	-
-	Fuel		Default emission factor	Lower	Upper	Default emission factor	Lower	Upper	Default emission factor	Lower	Upper							Orimul						21.0		18.9	23.3	_
_	Crude	Oil	73 300	71 000	75 500	r 3	1	10	0.6	0.2	2	-						Natural	Gas Liqui	ids				17.5		15.9	19.2	
	Orimu		r 77 000	69 300	85 400	r 3	1	10	0.6	0.2	2							Motor	Gasoline					18.9		18.4	19.9	
-	Natura Liquid		r 64 200	58 300	70 400	r 3	1	10	0.6	0.2	2							Aviatio	n Gasoline	e				19.1		18.4	19.9	_
		Motor Gasoline	r 69 300	67 500	73 000	r 3	1	10	0.6	0.2	2							2006 II	PCC Guio	delines for	Nationa	al Greenhou	ise Gas In	ventories,	Volume 2	Energy,	+ , Chapter 1:	. Ir
5	Gasoline	Aviation Gasoline	r 70 000	67 500	73 000	r 3	1	10	0.6	0.2	2															0,0		
<u>'</u>		Jet Gasoline	r 70 000	67 500	73 000	r 3	1	10	0.6	0.2	2																	
_	Jet Ker		r 71 500	69 700	74 400	r 3	1	10	0.6	0.2	2	_											TABLE 1.4	1				
	Shale	Kerosene Dil	71 900 73 300	70 800 67 800	73 700 79 200	r 3 r 3	1	10	0.6	0.2	2	-									DEFAU	LT CO <sub>2</sub> EMISS			SUSTION 1			
		iesel Oil	74 100	72 600	74 800	r 3	1	10	0.6	0.2	2	-												Default	Effec	ive CO <sub>2</sub> e	mission facto	r
		al Fuel Oil	77 400	75 500	78 800	r 3	1	10	0.6	0.2	2													carbon		(kg/I		
	Liquef Petrole Ethane	ied rum Gases	63 100 61 600	61 600 56 500	65 600 68 600	r 1 r 1	0.3	3	0.1	0.03	0.3	_						DEFAULT CO2 EMISSIOn           Fuel type English description         Default carbon content (kg/GJ)           A				Default	95% confidence interval					
	Naphtl		73 300	69 300	76 300	r 1 r 3	1	10	0.1	0.03	2	-													value <sup>3</sup> C=A*B*4			
_	Bitum	en	80 700	73 000	89 900	r 3	1	10	0.6	0.2	2											A		В	12*1000	" Lo	wer Up	per
	Lubric	ants sum Coke	73 300 r 97 500	71 900 82 900	75 200 115000	r 3	1	10	0.6	0.2	2							Crude O	a			20.0		1	73 300	71	100 75	500
	Refine					r 3			0.6		-	-						Orimulsi	on			21.0		1	77 000	69	300 85	400
	Feedst	ocks	73 300	68 900	76 600	r 3	1	10	0.6	0.2	2	_						Natural (	Gas Liquids	s		17.5		1	64 200	58	300 70	40
		Refinery Gas	n 57 600	48 200	69 000	r 1	0.3	3	0.1	0.03	0.3							. N	Iotor Gasol	line		18.9		1	69 300	67	500 73	00
		Paraffin Waxes	73 300	72 200	74 400	r 3	1	10	0.6	0.2	2							il A	viation Ga	soline		19.1		1	70 000	67	500 73	000
	Other Oil	White	73 300	72 200	74 400	r 3	1	10	0.6	0.2	3	_						, g	et Gasoline	•		19.1		1	70 000	67	500 73	000
1	õ	Spirit and SBP	73 300	72 200	74 400	1.5	1	10	0.0	0.2	,	_						Jet Kero	sene			19.5		1	71 500	69	700 74	400
		Other Petroleum Products	73 300	72 200	74 400	r 3	1	10	0.6	0.2	2							2006 I	PCC Guid	delines for	Nationa	al Greenhou	ise Gas In	ventories,	Volume 2	Energy,	, Chapter 1:	: Ir
	Anthra		98 300	94 600	101000	1	0.3	3	r 1.5	0.5	5																	
-	Coking		94 600	87 300	101000	1	0.3	3	r 1.5	0.5	5	_																
-	Coal	Bituminous	94 600	89 500	99 700	1	0.3	3	r 1.5	0.5	5	_						DEF	AULT NET	CALORIFIC V	ALUES (N	NCVs) AND LOV	TABLE 1.2 WER AND U		OF THE 95%	CONFIDEN	CE INTERVALS	, <b>1</b>
	Sub-B Coal	ituminous	96 100	92 800	100000	1	0.3	3	r 1.5	0.5	5												Ne	et calorific				-
	Lignite		101 000	90 900	115000	1	0.3	3	r 1.5	0.5	5							Fuel ty	pe Englisi	h description	1			lue (TJ/Gg)	Lo	wer	Uppe	c
	Sands	ale and Tar	107 000	90 200	125000	1	0.3	3	r 1.5	0.5	5							Crude C						42.3		).1	44.8	_
	Brown Brique		97 500	87 300	109000	n 1	0.3	3	r 1.5	0.5	5							Orimuls						27.5		7.5	28.3	
	Patent	Fuel	97 500	87 300	109000	1	0.3	3	n 1.5	0.5	5							Natural	Gas Liqui					44.2		).9	46.9	
		Coke Oven																B		fotor Gasoline				44.3		2.5	44.8	
	Coke	Coke and	r 107 000	95 700	119 000	1	0.3	3	r 1.5	0.5	5							Gasolii		viation Gasol	ine			44.3		2.5	44.8	_
-	ŏ	Lignite Coke																		et Gasoline				44.3		2.5	44.8	
	1	Gas Coke	r 107 000	95 700	119 000	r 1	0.3	3	0.1	0.03	0.3							Jet Kere	osene					44.1	4	2.0	45.0	

2006 IPCC Guidelines for National Greenhouse Gas Inventories, Volume 2: Energy, Chapter 1: Introduction

AX AY

IPCC default value: Table 1.2: Crude oil = 42.3 TJ/Gg, at 7.33 bbl per tonne, 1 bbl = 136.4 kg, 42.3 MJ/kg \* 136.4 kg = 5.771 GJ per bbl. Table 1.3: Crude = 20.0 kgC/GJ, thus 1 bbl = 20.0 kgC/GJ \* 5.7708 GJ/bbl = 115.416 kgC per bbl.

IPCC (2006) Guidelines 2006, Volume 2: Energy, Chapter 2: Stationary Combustion, Table 2.2

# Cell: C15

#### Comment: Rick Heede:

Sep2012: IPCC factors and values are used in this calculation; see following cell notes for details.

Previous note:

Carbon content of crude varies by API gravity and supply mixes but averages 20.23 kgC/million Btu (EIA 1605 reporting, EPA US Emissions reports, etc).

The typical barrel of oil is set by EIA (e.g., Annual Energy Review 2003, Table A2) at 5.80 million btu (US production) and varies for US imports between 5.802 and 5.971 over 1949-2003. We use 5.80 million btu per barrel in this report.

## Cell: D15

### Comment: Rick Heede:

The IPCC default value for crude oil is 20.0 kgC/GJ (range from 19.4 to 20.6 kgC/GJ). IPCC Guidelines 2006 Volume 2: Energy, chapter 1: Introduction, Table 1.3. Also listed as 56,100 kgC02/TJ in Table 2.2 at right. IPCC 2006 Guidelines vol 2, ch. 2: Stationary Combustion, Table 2.2.

### Cell: E15

# Comment: Rick Heede:

Calculated in Table 2.

### Cell: F15

### Comment: Rick Heede:

This result -- 117.33 kgC/bbl (Jan12) -- is slightly higher than the IPCC default value calculated from its 2006 Guidelines (Energy, Introduction, Tables 1.2 and 1.3): 115.42 kgC/bbl. IPCC default value: Table 1.2: Crude oil = 42.3 TJ/Gg, at 7.33 bbl per tonne, 1 bbl = 136.4 kg, 42.3 MJ/kg \* 136.4 kg = 5.7708 GJ per bbl. Table 1.3: Crude = 20.0 kgC/GJ, thus 1 bbl = 20.0 kgC/GJ \* 5.7708 GJ/bbl = 115.416 kgC per bbl.

Cell: C17

## Comment: Rick Heede:

Natural gas liquids are lighter than crude oil and have lower emission factors per unit volume (we focus here on EF on the basis of volume, rather than energy content, because oil and gas producers report production in bbl). The emission factor for butane (276.36 kgC02/bbl), ethane (181.44 kgC02/bbl), propane (234.78 kgC02/bbl), and natural gasoline (308.70 kgC02/bbl) averages to 250.32 kg C02/gallon. Crude oil's emission factor is 431.76 kg C02/gallon; the unweighted average NGL emission factor is thus 42 percent lower than crude oil. (data: U.S. Environmental Protection Agency (2011b) Emission Factors for Greenhouse Gas Inventories, epa.gov/climateleaders/ guidance/ghg-emissions.html);

EIA world production data for 1980-2012 show that Natural Gas Plant Liquids (NGPLs) comprise an average of 8.16 percent of total crude oil, lease condensate, and NGPLs for 1980-2012. The formula for the adjustment to crude oil emission factor (115.67 kgC/bbl) is as follows: 0.0816 \* (1-0.42044), which lowers the emission factor for combined crude oil and NGL to 110.20 kgC/bbl, or 403.80 kgC02/bbl.

# Cell: C19

### Comment: Rick Heede:

Dec2012: CMS does add company fuel and emissions to attributed entity emissions, since producers vary in their inputs of own fuels in production, transportation, shipping, processing, refining, and other direct Scope 1 emission sources. As estimated in the "Entity CDP Scopes 1-3" worksheet in the AncillaryCH4&CO2.xls, the emissions from own fuel inputs for the ten petroleum producers analyzed from the inventories submitted to the Carbon Disclosure Project for 2010 ranges from 4.8 percent (Hess) to 15.7 perent (ENI SpA) and averages 10.4 percent compared to emissions from oil and natural gas production. The preliminary conclusions in the previous notes below are reasonable approximations, though based on different data and methodology. ExxonMobil's estimated own fuel use in our analysis of the company's CDP submission for 2010 are equivalent to 12.9 percent of product emissions (79.4 MtCO2 compared to product emissions of 614 MtCO2).

## Cell: C21

#### Comment: Rick Heede:

Sep2012: CMS does not attribute vented CO2 in this worksheet. CMS does add a factor for vented CO2 from both oil and gas operations for each carbon major entity in the final entity summary worksheet. This value (as of Dec2012) is 0.408 kgC02/tCO2, or 0.041 percent.

### Cell: C23

### Comment: Rick Heede:

Sep2012: CMS does not attribute fugitive methane in this worksheet. CMS does add a factor for methane from both oil and gas operations for each carbon major entity in the final entity summary worksheet. This value (as of Dec2012) is 1.807 kgCH4/tC02 and 37.94 kgC02e/tC02, or 3.79 percent.

Previous note:

There is a paucity of measured data and even estimates of the amount of methane directly vented to the atmosphere from oil and natural gas operations. Certainly, most methane is not vented but flared for safety reasons, but there are numerous instances where fugitive leaks are routine. Moreover, methane was routinely vented rather than flared early in the 20th century. Accidental and uncapped releases of natural gas -- such as the 16-month-long event at one of Apache Corporation's fields in Texas from Oct1981 to Feb1983 \* -- are not uncommon. In addition, routine methane releases from tank purges, valve leakage, seal leakage, and so forth. Most such "routine" fugitive methane releases are attributed to natural gas operations.

\* See the "Gas Emissions factor Calc" and production worksheet for Apache Corp for details of the event and CMS carbon emissions estimate thereof.

Delucchi (2003) cites estimates off US offshore (including underwater) direct venting of natural gas of 48 cf to as high as 150 cf per barrel of oil produced. This 48 cf/bbl converts to 0.922 kg CH4 (19.2 g/cf of CH4, ignoring the nonmethane components) per barrel, and at 21x the GWP of CO2 is equivalent to 19.36 kgCO2e, or 5.28 kgCe/bbl. As a factor relative to the potential carbon dioxide in a bbl of oil (117.33 kgC/bbl, this represents 4.5 percent. This is twice

#### **Oil Emissions Factor Calc**

as high as the global methane rate used in the above calculation and in this worksheet, but then the US offshore natural gas venting rate is for offshore in the 1970s, and even that high rate has declined since.

### Cell: C25

### Comment: Rick Heede:

Sep2012: CMS does not attribute flared CO2 in this worksheet. CMS does add a factor for flared CO2 from both oil and gas operations for each carbon major entity in the final entity summary worksheet. This value (as of Dec2012) is 28.03 kgC02/tCO2, or 2.80 percent.

### Cell: C27

#### Comment: Rick Heede:

See the separate worksheet in this workbook ("Non-fuel uses"), in which CMS calculates (as of Dec2012) that 9.34 percent of total oil supplied to the U.S. economy (on average, 1980-2010, based on US data by EIA and EPA) is sequestered into petrochemicals and plastics, lubricants, waxes, polishes, petroleum coke, asphalt and road oils, etc.

Note that CMS has calculated, based on EIA (and secondarily, on IPCC) estimates, assumptions, and/or default values the fractions of non-fuel uses presumed to re-enter the atmosphere within a 20-year time horizon. Such as near-term oxidation or combustion of lubricants (either in the engines lubricated or post-collection and used as powerplant fuel), or as longer-term combustion of, say, petrochemicals and plastics in waste-to-energy plants, or the combustion of waxes, or the oxidation of the volatile components of polishes and paints).

The Oak Ridge National Lab's Carbon Dioxide Information Analysis Center (CDIAC)'s emissions database -- against which ultimate emissions estimated by CMS is compared year by year as well as cumulatively 1751-2010 -- makes the following footnote: "When calculating global total CO2 emissions from liquids, we have estimated that a quantity of liquids equivalent to 6.7% of liquids produced are not oxidized each year and another 1.5% passes through burners unoxidized or is otherwise spilled. Hence, 91.8% of annual liquid production is oxidized each year." http://cdiac.esd.ornl.gov/trends/emis/factors.htm

CMS averages the CDIAC and US carbon storage rates for crude oil & NGL production -(6.7 percent + 9.29 percent)/2 = 8.0 percent. This rate is applied here to account for the carbon produced in crude oil & NGL production that is not oxidised to CO2 and is deducted from the carbon coefficient for the average barrel of liquid fuel produced.

### Cell: C29

## Comment: Rick Heede:

IPCC 2006 Guidelines state a default oxidation factor of 100 percent; Chapter 1, Introduction, Table 1.4.

IPCC (1997) Guidelines for National Greenhouse Gas Inventories, vol 3, p. 1-28. Also EIA (2001) Emissions of Greenhouse Gases in the United States in 2000, Table A.3. While the EIA and EPA retain the use of this non-combustion factor, the IPCC's 2006 Guidelines appears to back away from its application. For example, IPCC's reference approach (Energy: chapter 6, p. 6-11): "Carbon Unoxidised During Fuel Combustion: A small part of the fuel carbon entering combustion escapes oxidation but the majority of this carbon is later oxidised in the atmosphere. It is assumed that the carbon that remains unoxidised (e.g. as soot or ash) is stored indefinitely. For the purposes of the Reference Approach, unless country-specific information is available, a default value of 1 (full oxidation) should be used."

CDIAC uses a factor of 1.5 percent for a combination of non-oxidised fuel and fuel spills. Per IPCC, fuel spills and most of non-oxidised fuel is, in fact, oxidised over a relatively short period. All in all, the deductions used by CMS -- carbon sequestered through non-fuel uses of liquid fuels at 8.0 percent, vs CDIAC's sum for the same two components at 8.2 percent.

## Cell: D36

#### Comment: Rick Heede:

Net calorific value of crude oil at 42.3 TJ/Gg (range from 40.1 to 44.8 TJ/Gg), IPCC 2006 Guidelines vol 2, ch. 1: Introduction, Table 1.2. Also lists natural gas as 48.0 TJ/Gg, and coal from 11.9 to 28.2 TJ/Gg.

### Cell: D37

### Comment: Rick Heede:

United Nations (2012) Energy Statistics Yearbook 2009, Jun, 696 pp. Table II: specific Gravities of Crude Petroleum. unstats.un.org/unsd/energy/yearbook/default.htm

### Cell: D41

#### Comment: Rick Heede:

The IPCC default value for crude oil is 20.0 kgC/GJ (range from 19.4 to 20.6 kgC/GJ). IPCC Guidelines 2006 Volume 2: Energy, chapter 1: Introduction, Table 1.3. Also listed as 56,100 kgC02/TJ in Table 2.2 at right. IPCC 2006 Guidelines vol 2, ch. 2: Stationary Combustion, Table 2.2.

## Cell: D42

## Comment: Rick Heede:

Calculated result. Based on IPCC default value for net calorific value (42.3 GJ/Tonne) divided by 7.3137 bbl /tonne. The result is dependent on the specific gravity, which the UN (Energy Statistics Yearbook, 2009, Appendix, "unspecified" oil, values for which varies from a high of 0.961 in Suriname to a low of 0.724 in Indonesia). Crude oil from Texas (45 GJ/t) would yield 6.25 GJ/bbl. Other unofficial sources put the average value at ~6.1 GJ/bbl (wikipedia).

### Cell: 150

Comment: Rick Heede:

Oil Emissions Factor Calc

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